



EICAS Automazione S.p.A

# The innovative methodology and the ACODUASIS project

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One step further in the automatic control design - 3 October 2005



# THEORETICAL FUNDAMENTALS

## GAP BETWEEN THEORY AND PRACTICE

### THEORY

SOPHISTICATED AND POWERFUL CONTROL ALGORITHMS  
MAY BE DESIGNED FOR “**DYNAMIC SYSTEMS**”  
BUT THEY ARE NOT USED IN PRACTICE

### PRACTICE

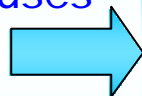
SIMPLE CLOSED LOOP CONTROL ALGORITHMS (SUCH AS  
P.I.D.) MAY BE SUCCESSFULLY IMPLEMENTED BY  
PERFORMING AN EXPERIMENTAL TUNING HAVING  
ONLY A RAW KNOWLEDGE OF THE “**PLANT**” DYNAMICS





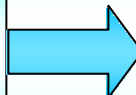
# THEORETICAL FUNDAMENTALS

Input  
causes

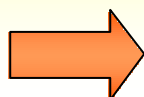


**PLANT**

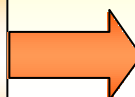
Output  
effects



**It is an object belonging  
to the real world**



**DYNAMIC  
SYSTEM**



**It is an object belonging  
to the mathematical world**

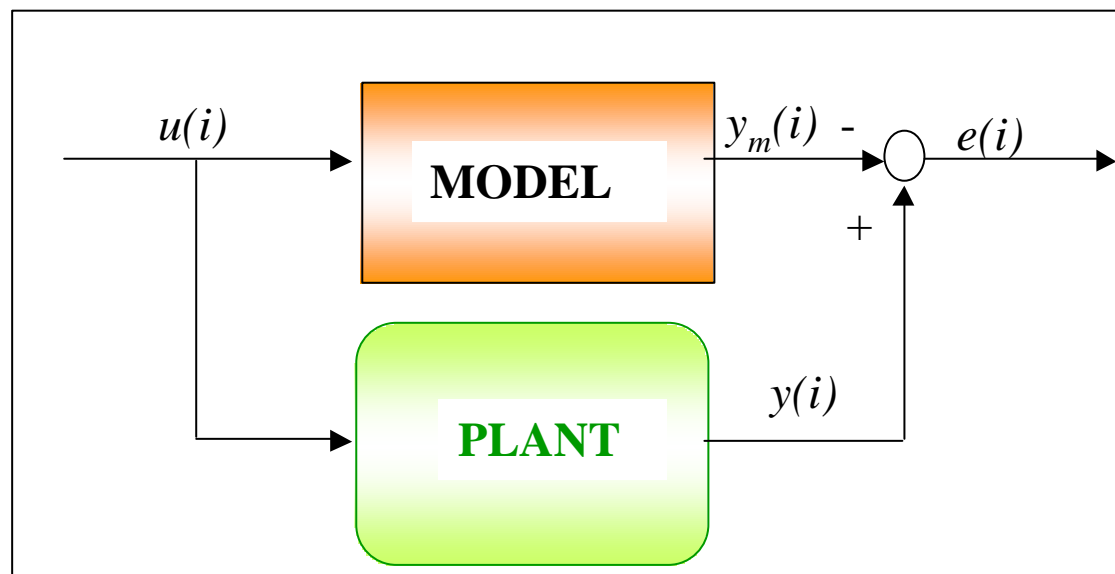
See  
"DYNAMIC SYSTEMS"  
according to the KALMAN definition  
1969



# THEORETICAL FUNDAMENTALS

## PLANT-MODEL UNCERTAINTY

Models can give only an approximate description of the related plant dynamics



A plant-model uncertainty always exists, which causes an error  $e(i)=y(i)-y_m(i)$ .

The plant-model uncertainty is said to be "NORM BOUNDED"

$\exists$  finite **E** and **D**

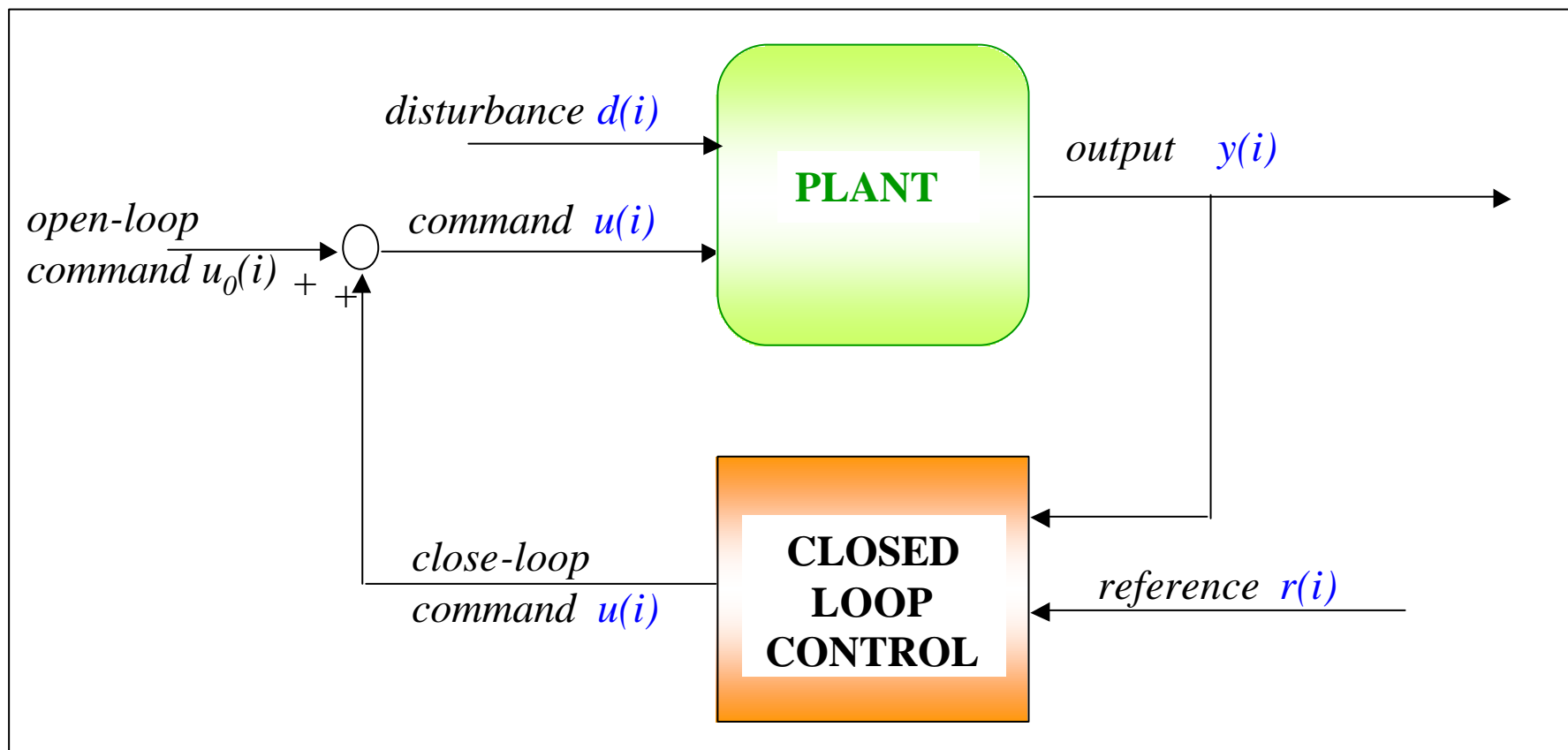
$$\|y - y_m\| < E \|y_m\| + D$$

$\forall u(i) \in U$  and  $\forall$  admissible operating conditions



# THEORETICAL FUNDAMENTALS

## CONTROL PERFORMANCE DEFINITION



attenuation factor  $Q$

$$||r-y|| < Q ||r-y_0||$$

Where  $y_0$  denotes the plant output in the absence of closed loop control, that is for  $u(i)=0$



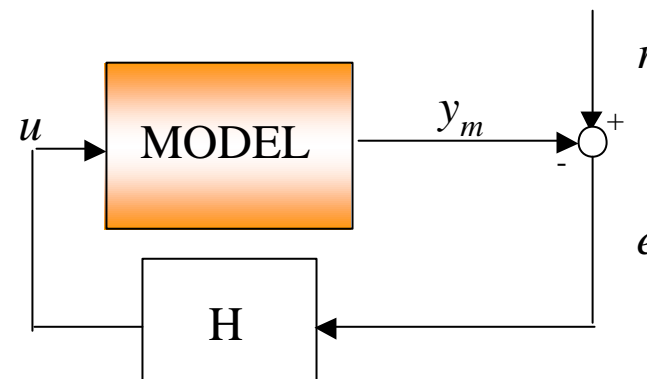
# THEORETICAL FUNDAMENTALS

## THE FUNDAMENTAL THEOREM

DONATI - CARLUCCI [1975] & DONATI - VALLAURI [1984]

If

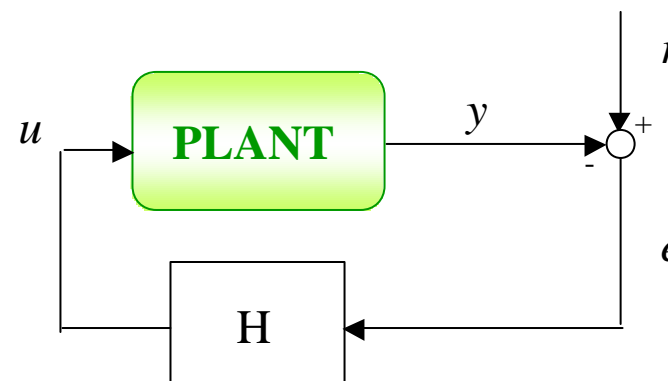
- $\exists$  a controller  $H$  such that  
 $\|e\| < Q \|r\| \quad \forall r \in \mathbb{R}$
- $E < 1/(1-Q)$



Then the same controller applied to the plant is stable and produces an attenuation of a factor  $Q^*$

$$Q^* < \frac{Q}{1 - E(1 + Q)}$$

Where  $\|e\| < Q^* \|r\| \quad \forall r \in \mathbb{R}$





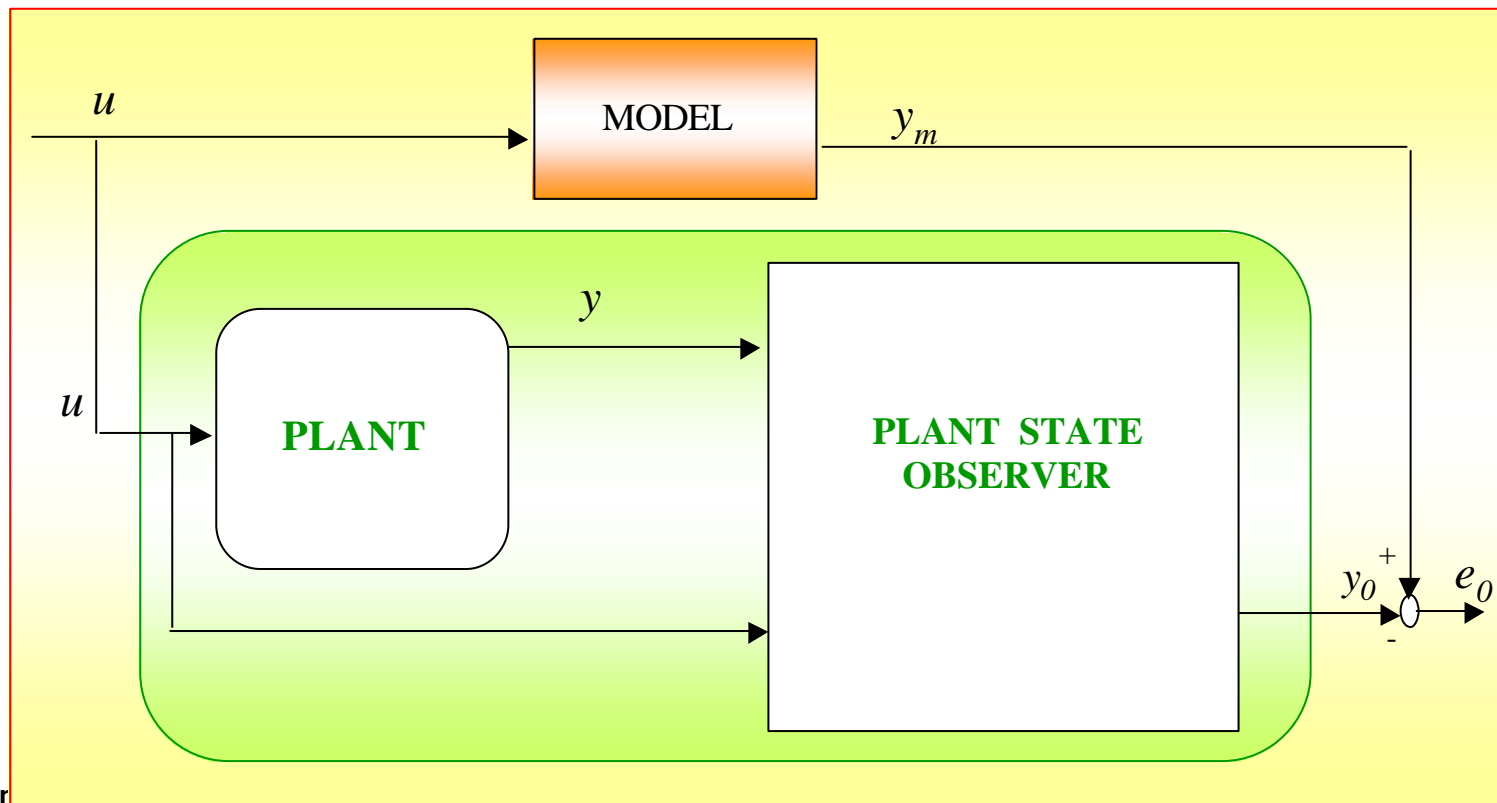
# THEORETICAL FUNDAMENTALS

## THE FUNDAMENTAL THEOREM

When the uncertainty is evaluated in the whole output Banach space, it appears impossible to build models of physical plants within the constraint

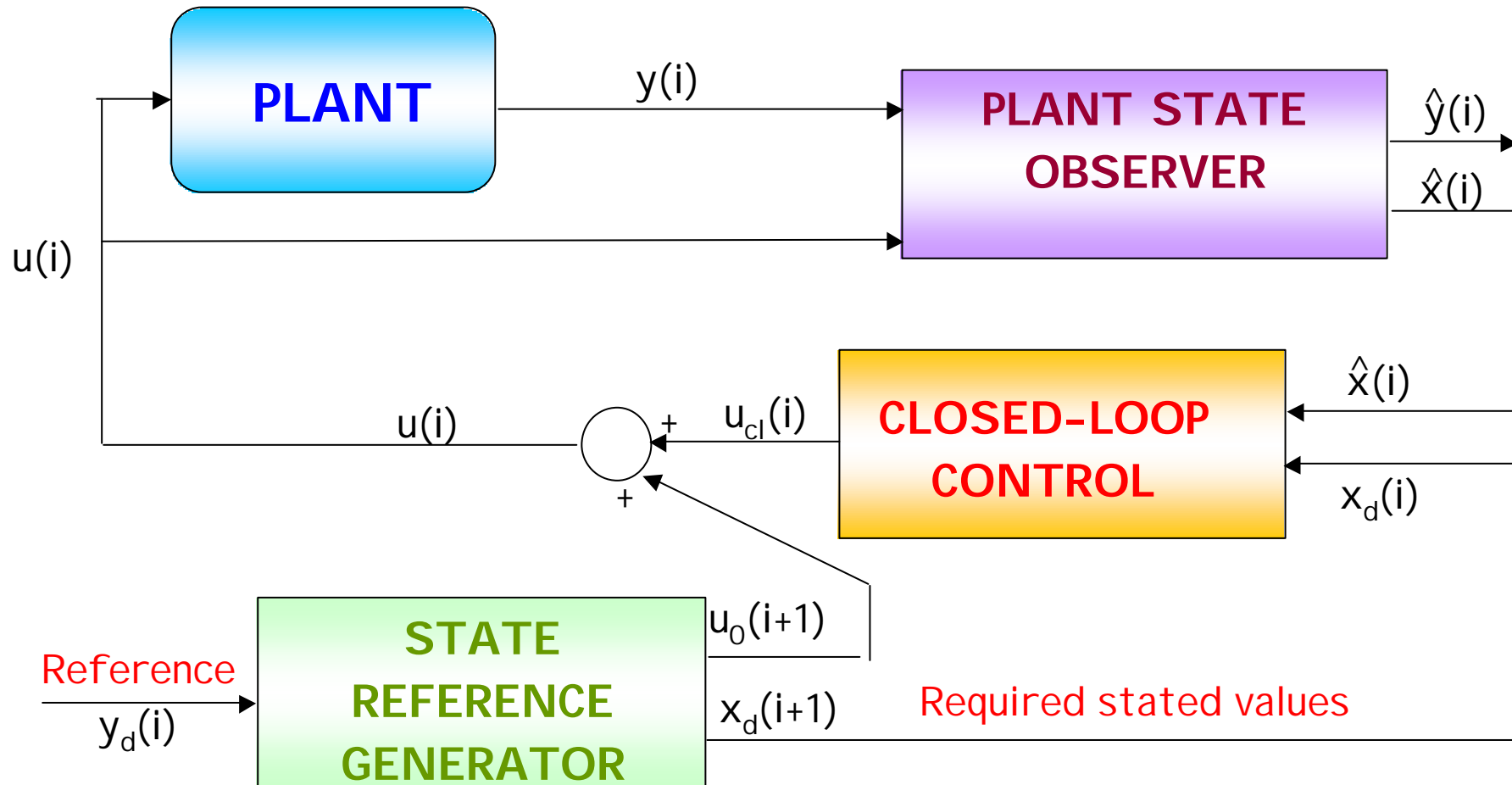
$$E < 1$$

*but it is possible to satisfy the above condition when  
bounded frequency domains are considered*





# THE EICAS CONTROL DESIGN APPROACH



REMARK - THE GUARANTEED PERFORMANCE IS RELATED TO

$$|| x_d(i) - \hat{x}(i) ||$$





# THE EICAS CONTROL DESIGN APPROACH

THE GUARANTEED PERFORMANCE IS RELATED TO THE STATE CONTROL

$$\boxed{\text{closed loop error } || x_d(i) - \hat{x}(i) ||} < Q^* \boxed{|| x_d(i) - \hat{x}_o(i) || \text{ open loop error}}$$

The plant control error  $|| y_d(i) - y(i) ||$  is the resulting effect of two error causes:

- The control error  $|| y_d(i) - y(i) ||$ , of the observed output, which can be made so small as required
- the observer error  $|| y(i) - \hat{y}(i) ||$ , which depends on the observer design but cannot be made as small as required

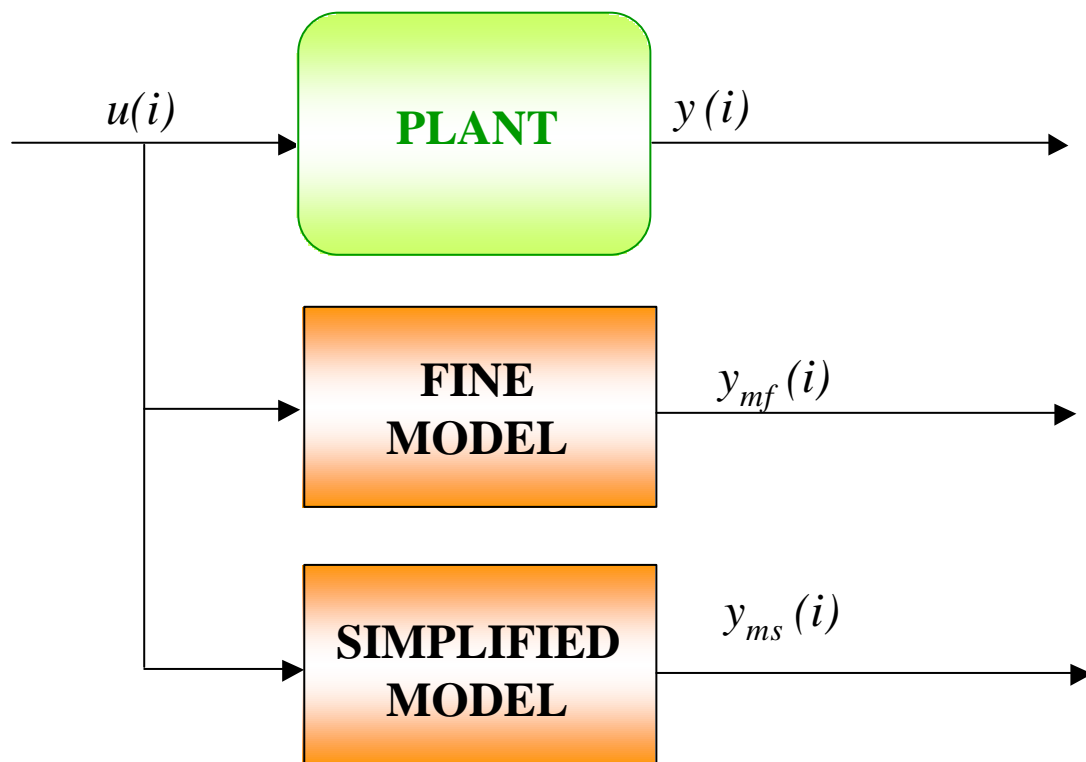
## CONCLUSIONS:

- the plant control error is “practically” given by the observer error alone
- the observer design is the most critical point in the plant control design





## THE TWO MODELS APPROACH





two different models of the plant are used to design the plant control algorithm.

The “plant simplified model” is the main basis of the control design.

The “plant fine model” is strictly related to the previous one, having the aim of showing the limit of the field within which the “plant simplified model” gives a description of the plant behavior sufficiently accurate from the point of view of the control design.





The **plant control design** consists of two main steps: the state observer design and the state controller design.

The **state controller design** is performed only on the basis of the “plant simplified model” with the aim of getting any stated attenuation factor  $Q_0$

The **state observer design** is also performed on the basis of the “plant simplified model”, but with requirements derived from the “plant fine model” analysis.



The **control guaranteed performance** is evaluated by a set of trials performed in a simulated environment by applying the designed control to the "plant fine model".

In order to **optimize** the control performance a tuning of the control parameters can also be performed in the same environment simulated above.





# THE CONTROL DESIGN APPROACH

1. "REQUIREMENT SPECIFICATIONS"
2. PLANT SIMPLIFIED MODEL
3. PLANT FINE MODEL
4. ACCURACY LIMIT VERIFICATION ( $E < 1$ )
5. CONTROL DESIGN



The experience has proved that:

- plant controls designed according to the described methodology **do not need experimental parameter tuning in field**
- the control performance obtained by sophisticated modern controls is better than the one obtained by means of simple controls experimentally tuned.





## CONCLUSIONS

### FROM THE ACODUASIS EXPERIENCE

The most critical step in the plant control design is the choice of the plant simplified model and of the related plant fine model.

Such a model selection requires deep expertise in designing controls for the specific technological sector considered.

Once the two models have been selected, the following control design steps can be largely automated and supported by a professional software tool like EICASLAB

